

Electrochemical Chlorine-Free AC Disinfection of Water Contaminated with Salmonella Typhimurium Bacteria

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Abstract—Deionized (DI) water contaminated with Salmonella Typhimurium (*S. Typhimurium*) bacteria was disinfected by alternating current. Ammonium sulfate was used as electrolyte. Disinfection was carried out in the circulation system including an electrochemical cell with stainless steel electrodes. The process efficiency was estimated and the number of killed bacteria was directly proportional to the water treatment time and concentration of hydroxyl radicals generated by electrolysis. The presence of OH radicals was detected with N,N-dimethyl-p-nitrosoaniline (RNO) used as a spin trap. Similar experiments were carried out with water remaining after poultry washing at poultry farms and additionally contaminated with *S. Typhimurium* bacteria. Measures were recommended to increase the process efficiency and decrease the water treatment time.

Key words: water disinfection with alternating current, electrochemical treatment, hydroxyl radicals, spin trap, kinetic model

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INTRODUCTION

Sewage water contains numerous microorganisms. There are numerous methods to reduce the number of infection components to an acceptable level for drainage to any water pools [1]. Earlier, the chlorination method was traditionally used; in recent years, ozone treatment, ultraviolet irradiation, and various electrochemical processes are applied. Selection of the disinfection method significantly depends upon the cost of required energy, especially in the cases, where large quantities of water should be treated.

Salmonella Typhimurium (*S. Typhimurium*) bacteria are classified as the most dangerous microorganisms causing serious intestinal disorders of humans. Food products of animal and vegetable origin are often infected with *S. Typhimurium* bacteria. Water remaining after poultry washing at poultry farms (poultry water) is also often infected with these bacteria. Recently, poultry water was disinfected by such chemical methods as chlorination [2], ozonation [3], and others [4]. The disadvantages of these methods include potential formation and accumulation of toxic chemical products as, for example, in the case of chlorination or high cost as in the case of ozonation [5].

Electrochemical treatment of water, including poultry water became interesting relatively recently

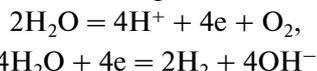
[1, 6–12]. The authors of [1] found that effective electrolytic water treatment using NaCl electrolyte is accompanied by generating significant quantities of elementary chlorine, hypochlorite, and, probably, chlorate and requires a high initial concentration of NaCl (over 0.15%). At such concentration, chloride anions cause corrosion of any bimetal parts of water systems, for example, water distributors, cooling towers, etc. Replacement of chloride anions with phosphates, nitrates, sulfates, or carbonates, which do not cause corrosion, is more favorable with respect to the equipment operation costs and increases profitability of the electrochemical water sterilization process.

The mechanism of electrochemical disinfection depends upon numerous parameters, including the nature of electrolyte. The authors of [6, 13, 14] calculated the number of *S. Typhimurium* bacteria in NaCl, Na₂SO₄, and Na₃PO₄ solutions subjected to low-voltage and low-current electrolysis. Already in five-minutes, this treatment was shown to reduce the concentration of live *S. Typhimurium* bacteria by one or two orders of magnitude.

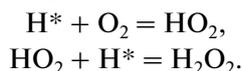
The authors of [15–17] studied the electrochemical disinfection mechanism for *E. coli* B bacteria in NaCl, NaNO₃, and Na₂SO₄ solutions. The disinfection efficiency of electrolysis was close to that of ozonation, i.e., much higher than that of ordinary chlorination. Electrochemical disinfection was shown to kill bacte-

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ria not by electric field. In the opinion of the authors of [18], the major contribution to the disinfection effect is made by generation of hydroxyl radicals. The formation mechanism of OH radicals in electrolysis of aqueous solutions was discussed by the authors of [19–21]. They showed, in particular, that the generally accepted schemes of anodic oxidation and cathodic reduction are simplified for the reactions:



Formation of atomic hydrogen (H^*) is one of the intermediate stages in the course of molecular hydrogen formation in the reaction of cathodic reduction. Here a part of atomic hydrogen initiates the following sequence of reactions:



In the cases, where electrodes are made of metal (M), hydrogen peroxide takes part in the reaction generating hydroxyl radicals:



The life time of hydroxyl radicals is too short for their identification by ESR method. Nevertheless, an effective method for detection of OH radicals was suggested by the authors of [21]. They analyzed the interaction products of OH radicals with tert-butyl nitron in electrolysis of potassium chlorate solutions. The generated long-living radicals were detected by ESR method.

In addition to OH radicals, the disinfection process may involve also other intermediate highly active compounds such as $\cdot\text{O}_2^-$ anion radicals. In the case of sulfate electrolyte [22], there may be persulfate and sulfate radicals. In electrolysis of phosphate buffer [23, 24], bacteria are killed due to formation of hydrogen peroxide.

Our earlier studies [25, 26] represent the results from electrochemical disinfection of deionized (DI) water contaminated with *E. coli* B and containing $(\text{NH}_4)_2\text{SO}_4$ as electrolyte. We suggested a kinetic model for elimination of bacteria and a quantitative method describing the rate of interaction between hydroxyl radicals and bacteria and considered the effects of such parameters as treatment time, electrolyte concentration, and initial concentration of bacteria. In this work, we analyzed the results of a similar study carried out for DI water and poultry water contaminated with a high concentration of *S. Typhimurium* bacteria.

EXPERIMENTAL

We used N,N-dimethyl-p-nitrosoaniline (RNO) used as a spin trap for hydroxyl radicals. The concentration of OH radicals resulting from electrolysis was estimated with a spectrophotometer by the change in the RNO optical absorption spectral intensity with the peak at 440 nm. The solutions of DI water contained

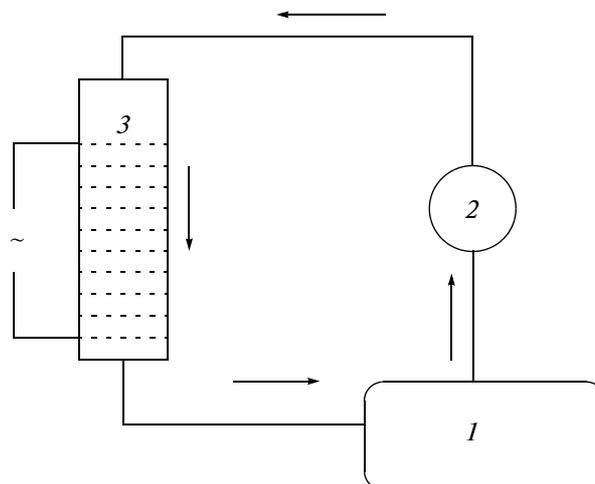


Fig. 1. Laboratory electrochemical water disinfection device: (1) pump, (2) water flow meter, (3) plastic electrochemical cell; parallel set of ten stainless steel net electrodes (5.5 cm diameter) with 3 mm intervals.

the $(\text{NH}_4)_2\text{SO}_4$ electrolyte concentration of 0.025 to 0.5% and RNO concentration of 0.0027 to 0.003% (1.8×10^{-6} to 2.0×10^{-6} M). Our selection of $(\text{NH}_4)_2\text{SO}_4$ as electrolyte was accounted for by the fact that it is relatively harmless and cheap. The poultry water was provided by the experimental poultry farm at the University of Arkansas (Fayetteville, Arkansas, USA). Before electrolysis, this water was diluted with the same volume of DI water containing the necessary quantities of $(\text{NH}_4)_2\text{SO}_4$ and RNO. According to the results of microbiological analysis, the population of *S. Typhimurium* bacteria in the prepared solution was below the detection level. We prepared the solutions of *S. Typhimurium* bacteria with various concentrations by dilution of water with highly concentrated suspension containing approximately 42×10^6 cfu/ml of bacteria.

Our experimental water disinfection device is represented in Fig. 1. We found that alternating current of 0.21 A (50 Hz frequency) corresponding to the current density of 60 mA/cm^2 does not cause corrosion of steel electrodes in the selected range of ammonium sulfate concentrations. We maintained the constant current density by selecting the initial voltage in the range from 40 to 170 V with respect to the electrolyte concentration.

Before starting each experiment, the laboratory device was disinfected for 20 min with hot water flow at the temperature of 75 to 80°C. The initial temperature of the treated water was 20°C. The water flow rate through the electrochemical cell was 40 l/min. The portions of 10 ml were sampled through the open cover of electrochemical cell and stored at 4°C for microbiological analysis. The colonies of *S. Typhimurium* were counted after incubation for 48 h at 35°C.

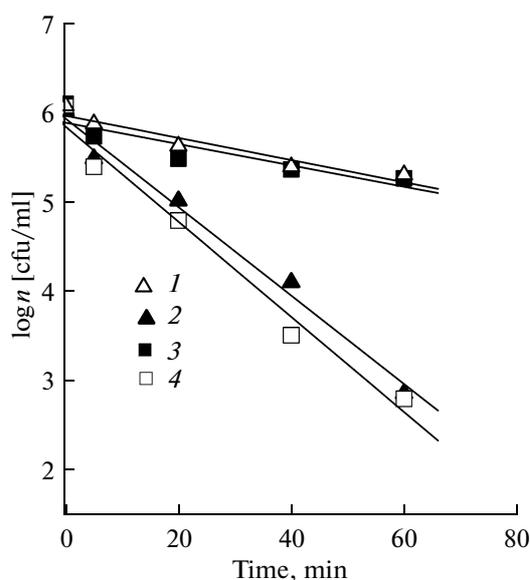


Fig. 2. Live *S. Typhimurium* bacteria count vs. disinfection time in $(\text{NH}_4)_2\text{SO}_4$ solutions with concentrations of 0.025% (1, 2) and 0.05% (3, 4) without electrolysis (1, 3) and with electrolysis (2, 4).

RESULTS AND DISCUSSION

DI water contaminated with *S. Typhimurium*

Figure 2 represents a typical curve of live bacteria concentration in solution vs. electric current treatment time. Our analysis of experimental data enables to make to conclusions. First, without electric current, no addition of $(\text{NH}_4)_2\text{SO}_4$ and RNO to DI water contaminated with *S. Typhimurium* causes any significant bactericidal effect. Second, if electric current is applied, the number of live bacteria vs. treatment time can be described with a linear logarithmic curve. To describe the process of electrolysis, we used a modified kinetic model designed for the disinfection of natural water contaminated with coliforms [15].

According to this model, the initial number of bacteria (n_0) and the current number of bacteria (n) at time moment t are interrelated as follows:

$$\log n = \log n_0 - kt, \quad (1)$$

where k is the factor depending on the current density for the constant volume of water to be disinfected and constant surface area of the electrodes.

The diagram in Fig. 2 enables to calculate factor k and to determine such essential parameter of disinfection process as the minimum time t_d , which is necessary to decrease the concentration of bacteria to $n = 1$. With respect to calculation of the bacteria population in the selected dimension, such low concentration should be considered as negligibly small. Therefore, t_d can be referred to as the time required for complete elimination of bacteria. It corresponds to the intersection point of the experimental line with the time axis. Table 1 represents the parameters of k and t_d calculated for each concentration of electrolyte.

The contaminated water flow through the electrochemical cell without the applied voltage slightly decreases the population of bacteria, which becomes noticeable after 30 min experiment. A similar effect was earlier noted for DI water contaminated with *E. coli* B [26] and seems to be accounted for by the known biocide effect of cavitation to microorganisms.

Poultry water contaminated with *S. Typhimurium*

Our electrochemical experiments with poultry water contaminated with *S. Typhimurium* bacteria were carried out under the same conditions as our experiments with DI water. First, as in the case of DI water, electrochemical disinfection of poultry water takes place far more effectively than water flow through electrodes under no voltage. Second, the live bacteria count vs. water treatment time is described with logarithmic curve.

Compare factor k and time t_d for poultry water with the corresponding data for DI water in Table 1. We can

Table 1. Factor k and complete disinfection time t_d calculated for linear model (equation (1)) for electrolysis of aqueous *S. Typhimurium* solutions

| Electrolyte concentration | <i>S. Typhimurium</i> disinfection media | $\log n_0$ [cfu/ml] | k | t_d , min |
|---------------------------|--|---------------------|--------|-------------|
| 0.025 | DI water | 6.01 | 0.0499 | 120.2 |
| | poultry water | 5.76 | 0.0448 | 128.6 |
| 0.05 | DI water | 6.06 | 0.0550 | 110.1 |
| | poultry water | 5.68 | 0.0464 | 122.3 |
| 0.2 | DI water | 6.13 | 0.0565 | 108.5 |
| | poultry water | 5.63 | 0.0472 | 119.2 |
| 0.5 | DI water | 6.21 | 0.0634 | 98.0 |
| | poultry water | 5.59 | 0.0503 | 111.2 |

see that achievement of complete disinfection by electrochemical treatment of *S. Typhimurium* bacteria in poultry water requires more time than in the case of DI water.

Kinetics of interaction between OH radicals and *S. Typhimurium* bacteria

Generation of OH radicals by electrochemical treatment of contaminated water was successfully used for oxidation of organic compounds, for example, phenols [28]. The advantages of RNO used as a spin trap are accounted for by high selectivity of the reaction of interaction between RNO and OH radicals. Consider the reactions of OH radicals spending in the course of electrolysis. The interaction scheme can be represented as follows:

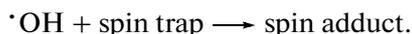
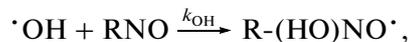


Figure 3 shows the change in the absorption spectra of RNO in $(\text{NH}_4)_2\text{SO}_4$ aqueous solution contaminated with *S. Typhimurium* under the conditions of electrolysis. As we see, a solution flow through the zero-current electrolytic cell only slightly decreases the optical density at 440 nm. Under the conditions of electrolysis, the optical density changes rapidly. It decreases far more rapidly if electrolysis takes place in the bacteria-free solution. These results apparently evidence formation of OH radicals.

We neglect potential occurrence of other reactions involving hydroxyl radicals, excepting elimination of bacteria and interaction with RNO. Then expenditure of OH radicals in electrochemical treatment can be described as follows [26]:



We use the kinetic model suggested for description of two competing reactions [28]:

$$1/G_t = 1/G_o \{1 + (k'_{\text{OH}}[\text{B}]) / (k_{\text{OH}}[\text{RNO}])\}, \quad (2)$$

where G_t is the RNO decoloration rate in the presence of bacteria, G_o is the RNO decoloration rate in the absence of bacteria, $[\text{B}]$ is the concentration of bacteria in solution, $[\text{RNO}]$ is the RNO concentration in solution, and k'_{OH} and k_{OH} are the relevant reaction rate constants.

Like in the case of DI water, voltage applied to poultry water sharply decreases the RNO optical density at 440 nm. Compare the kinetic characteristics of RNO interaction with hydroxyl radicals in DI water and poultry water. For this calculation, we selected the electrolyte concentration of 0.2% and various initial concentrations of *S. Typhimurium* (Table 2). The RNO concentration was measured after 40 min treatment of water. The $1/G_t$ vs. $[\text{B}]/[\text{RNO}]$ is a linear relationship with the slope of $1/G_o(k'_{\text{OH}}/k_{\text{OH}})$. The radical-bacteria interaction rate constant k'_{OH} was calcu-

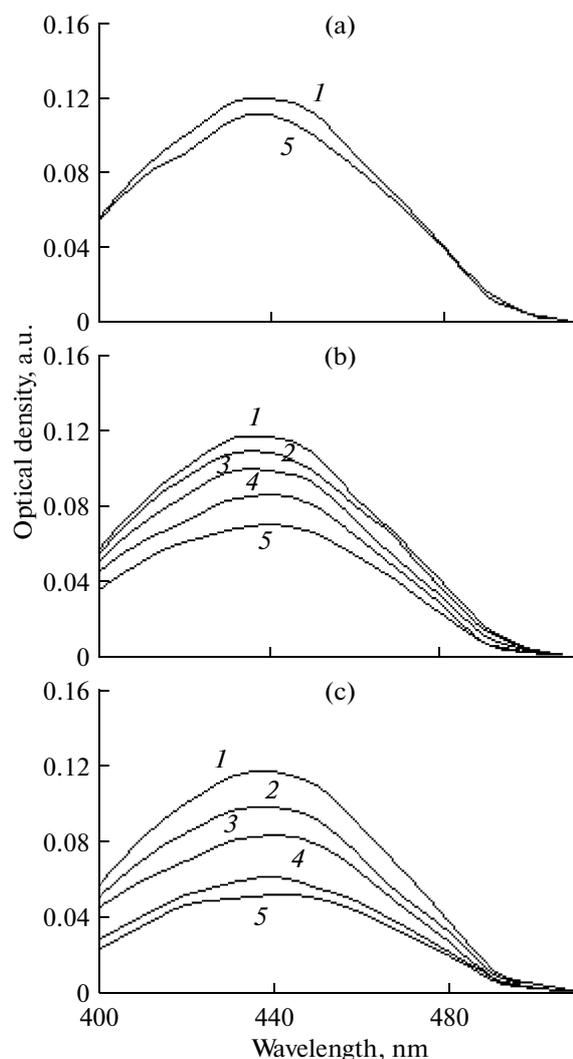


Fig. 3. Absorption spectra of RNO in DI water contaminated with *S. Typhimurium* before (1) and after flow through electrochemical cell for 5 (2), 20 (3), 40 (4), 60 (5) min; water treated without voltage (a), under voltage (b), under voltage in bacteria-free solution (c).

lated in the assumption that the RNO-OH radical reaction rate constant is $1.2 \times 10^{10} \text{ mol}^{-1} \text{ s}^{-1}$ [4]. Thus calculated values of k'_{OH} for DI water and poultry water are represented in Table 2 along with the values of constant k and time t_d for both kinds of water as calculated by equation (1). We see that the bacteria elimination rate in DI water is higher than that in poultry water.

Therefore, disinfection of poultry water is a slower process than disinfection of DI water. This conclusion follows from comparison of the bacteria elimination rate k'_{OH} and agrees with the determined time t_d required for complete disinfection of water. As follows from [29], the bacteria elimination rate under electrochemical treatment of *S. Typhimurium* suspensions is

Table 2. Factor k and complete disinfection time t_d calculated by equation (1) and *S. Typhimurium* elimination rate constants calculated by equation (2)

| <i>S. Typhimurium</i> disinfection media | $\log n_0$ [cfu/ml] | k | t_d , min | k'_{OH} , cfu s ⁻¹ |
|--|---------------------|-------|-------------|---------------------------------|
| DI water | 6.13 | 0.057 | 109 | 3.9×10^6 |
| DI water | 6.32 | 0.055 | 116 | |
| DI water | 6.43 | 0.053 | 122 | |
| DI water | 6.85 | 0.055 | 125 | |
| poultry water | 5.63 | 0.047 | 119 | 1.7×10^6 |
| poultry water | 5.76 | 0.047 | 124 | |
| poultry water | 5.89 | 0.046 | 127 | |
| poultry water | 6.05 | 0.046 | 130 | |

higher in DI water than that in poultry water. This difference was accounted for by the fact that poultry water contains additionally blood cells, fat micelles, and other organic substances, which can coat the cells of bacteria and thus protect them from the effect of radicals. Such explanation seems to be true also for interpretation of the results represented in this work.

Comparison of interaction kinetics of hydroxyl radicals with *S. Typhimurium* bacteria

Table 3 represents the results from electrochemical treatment of DI water contaminated with bacteria of two species. All the measurements were carried out with the same electrolyte in the same concentration under the same conditions of AC treatment. Apparently, for approximately the same initial concentration of bacteria (deviation not exceeding 3%), complete disinfection in the case of *E. coli* B needs less time than in the case of

S. Typhimurium. Our conclusion that disinfection of *S. Typhimurium* is a slower process as compared to that of *E. coli* B is confirmed with the bacteria elimination rate constants k'_{OH} . These constants were calculated in [26] as 3.91×10^6 and 6.01×10^6 cfu s⁻¹, respectively.

The efficiency of electrochemical disinfection can be enhanced also by varying such parameters as water volume and flow rate through electrochemical cell as well by changing the nature of the electrode materials. The energy loss of this process decrease at a lower electric resistance of the electrolyte solution, for example, for a shorter distance between electrodes, larger surface area, or higher electrolyte concentration. The process cost can be essentially decreased by selecting

Table 3. Complete water disinfection time t_d for various initial concentrations of *S. Typhimurium* and *E. coli* B bacteria

| Electrolyte concentration | Bacteria species in DI water* | $\log n_0$ | t_d , min |
|---------------------------|-------------------------------|------------|-------------|
| 0.025 | <i>S. typhimurium</i> | 6.01 | 120 |
| | <i>E. coli</i> B | 6.12 | 103 |
| 0.05 | <i>S. typhimurium</i> | 6.06 | 110 |
| | <i>E. coli</i> B | 6.10 | 96 |
| 0.2 | <i>S. typhimurium</i> | 6.13 | 109 |
| | <i>E. coli</i> B | 5.95 | 89 |
| 0.5 | <i>S. typhimurium</i> | 6.21 | 98 |
| | <i>E. coli</i> B | 6.23 | 89.3 |

* Disinfection data of DI water contaminated with *E. coli* B taken from [20].

the electrolyte, for example, if (NH₄)₂SO₄ is replaced with cheaper Na₂SO₄.

CONCLUSIONS

(1) Chlorine-free AC electrochemical disinfection with ammonium sulfate electrolyte is an effective method for disinfection of DI water contaminated with *S. Typhimurium* bacteria.

(2) If all other conditions are the same, disinfection of poultry water requires more time than disinfection of DI water.

(3) Use of N,N-dimethyl-p-nitrosoaniline as a spin trap experimentally confirmed formation of hydroxyl radicals in electrolysis of aqueous ammonium sulfate solutions. Hydroxyl radicals make an essential impact to the bactericidal process.

(4) Under the same electrolytic conditions, disinfection of DI water contaminated with *S. Typhimurium* bacteria takes more time than in the case of DI water contaminated with *E. coli* B. This conclusion is confirmed with the kinetic calculations for expenditure of hydroxyl radicals.

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